

# NITROGEN AND PHOSPHORUS: TREATMENT CONCEPTS

**CDM**

Anna Mehrotra, Ph.D.  
MehrotraAS@cdm.com

December 1, 2010

# Part II: Phosphorus

## Periodic Table of the Elements

1	IA																IIA																IIIA																IVA																VA																VIA																VIIA																O																																																																																																																																																																															
1	H																He																																																																																																																																																																																																																																																																															
2	Li																Be																B																C																N																O																F																Ne																																																																																																																																																																															
3	Na																Mg																Al																Si																P																S																Cl																Ar																																																																																																																																																																															
4	K																Ca																Sc																Ti																V																Cr																Mn																Fe																Co																Ni																Cu																Zn																Ga																Ge																As																Se																Br																Kr															
5	Rb																Sr																Y																Zr																Nb																Mo																Tc																Ru																Rh																Pd																Ag																Cd																In																Sn																Sb																Te																I																Xe															
6	Cs																Ba																*La																Hf																Ta																W																Re																Os																Ir																Pt																Au																Hg																Tl																Pb																Bi																Po																At																Rn															
7	Fr																Ra																+Ac																Rf																Ha																Sg																Ns																Hs																Mt																110																111																112																113																																																																																															

\* Lanthanide Series

+ Actinide Series

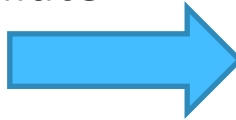
58	59	60	61	62	63	64	65	66	67	68	69	70	71
Ce	Pr	Nd	Pm	Sm	Eu	Gd	Tb	Dy	Ho	Er	Tm	Yb	Lu
90	91	92	93	94	95	96	97	98	99	100	101	102	103
Th	Pa	U	Np	Pu	Am	Cm	Bk	Cf	Es	Fm	Md	No	Lr

# Phosphorus Topics

- **Problems:** why remove?
- **Forms:** what is found in wastewater?
- **Removal concepts:** how is P removed from wastewater?
- **Process considerations:** what design and operational factors influence removal?
- Tying N & P removal together

# Why Remove Phosphorus?

- Ecological consequences:
  - Phosphorus may stimulate excess algae growth (eutrophication)
  - If nitrogen loading to water body decreased, phosphorus can become limiting



# Forms: Basic Categories

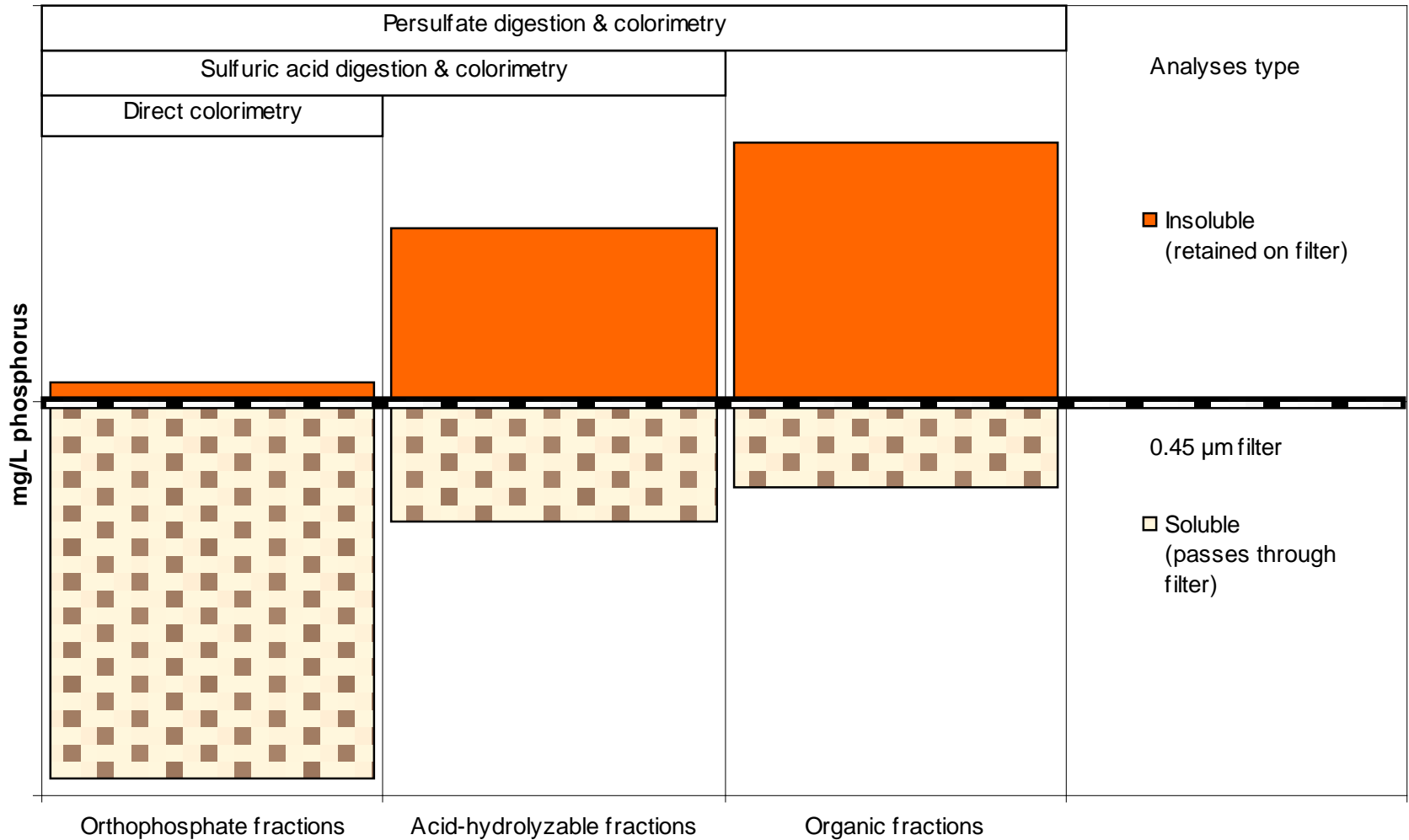
- Dissolved vs. particulate
- Organic vs. inorganic
- *No gas phase*

# Forms: Operational Definitions

- Defined by analytical method, not by chemical structure
- Two common methods:
  - EPA Method 365.2
  - Standard Methods 4500-P
- Three common colorimetric analyses:
  - Direct colorimetry
  - Sulfuric acid digestion/colorimetry
  - Persulfate digestion/colorimetry
- Filtered and unfiltered (typically 0.45  $\mu\text{m}$ )

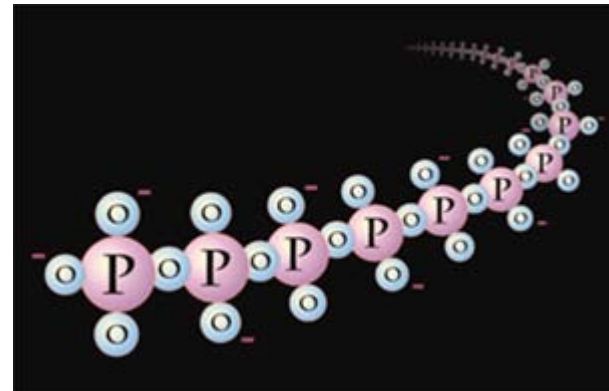


# Forms: Six P Fractions



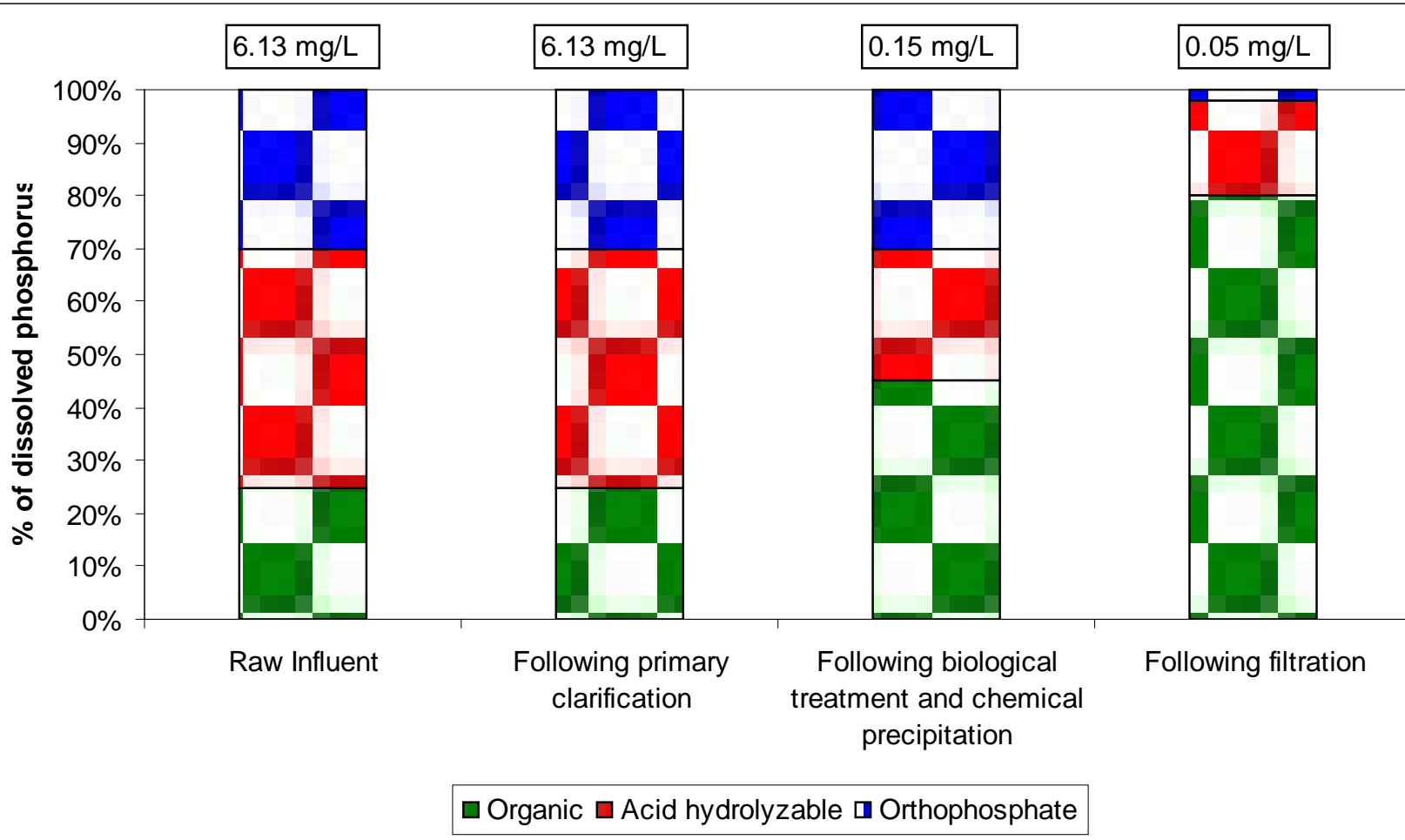
# Forms: Operational Definitions

- “Orthophosphate”
  - Mostly orthophosphate (“ortho-P”;  $\text{H}_2\text{PO}_4^-$  and  $\text{HPO}_4^{2-}$ )
  - Mostly dissolved
  - Highly reactive
- “Acid-hydrolyzable”
  - Mostly “condensed” phosphates: polyphosphates and metaphosphates
  - Dissolved and particulate
  - Somewhat reactive
- “Organic”
  - Phospholipids, nucleotides
  - Mostly particulate
  - Least reactive





# Forms: Dissolved P in WWTP



# Forms: Total and Soluble Reactive P

- Total (TP) = total, unfiltered, persulfate-digested result
- Soluble Reactive (SRP) = ortho-P  
= filtered, direct colorimetry result

# Forms: Typical Concentrations in Raw Domestic Wastewater

Form	Wastewater Strength		
	Strong	Medium	Weak
Total	12	7	4
Organic	4	2	1
Inorganic	8	5	3
Ortho-P	6	4	2

Ortho-P ~ 50% of TP

(Metcalf & Eddy)

# Removal Concepts: Basic Ideas

- What comes in must go out
  - Water
  - Solids
- Everything must be converted to solid form to be removed
  - Biological (biomass)
  - Chemical
- Remove solids
  - Sedimentation
  - Filtration
  - Membrane separation



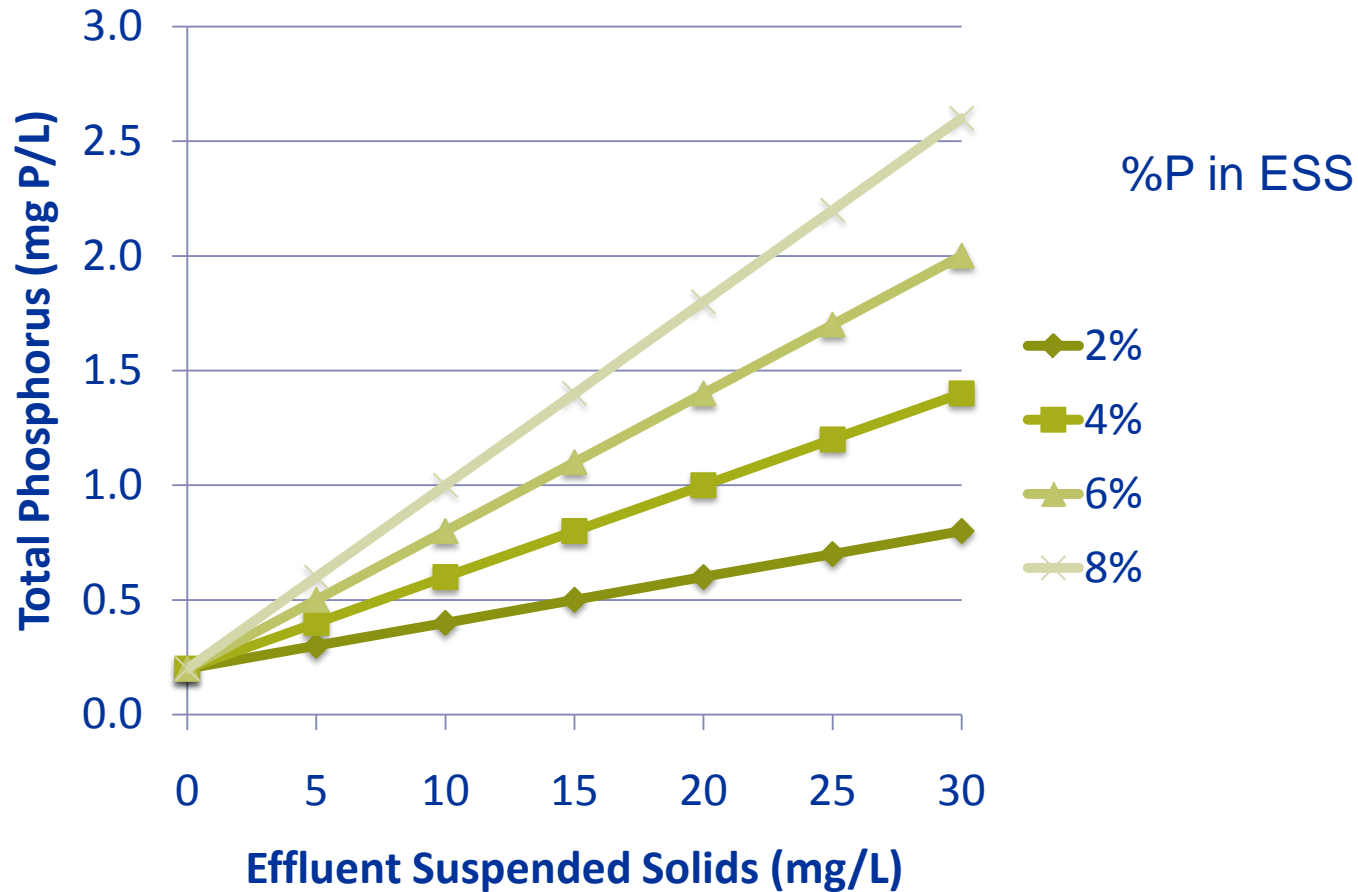
# Removal Concepts: Overview

- Inorganic, non-ortho-P converted to ortho-P: **hydrolysis**
- Ortho-P incorporated into biomass: **assimilation**
  - ➔ Increase P content in biomass with P storage with Bio-P
- Ortho-P removed by reaction with metal salts: **chemical precipitation**

# Removal Concepts: Incorporation into Biomass

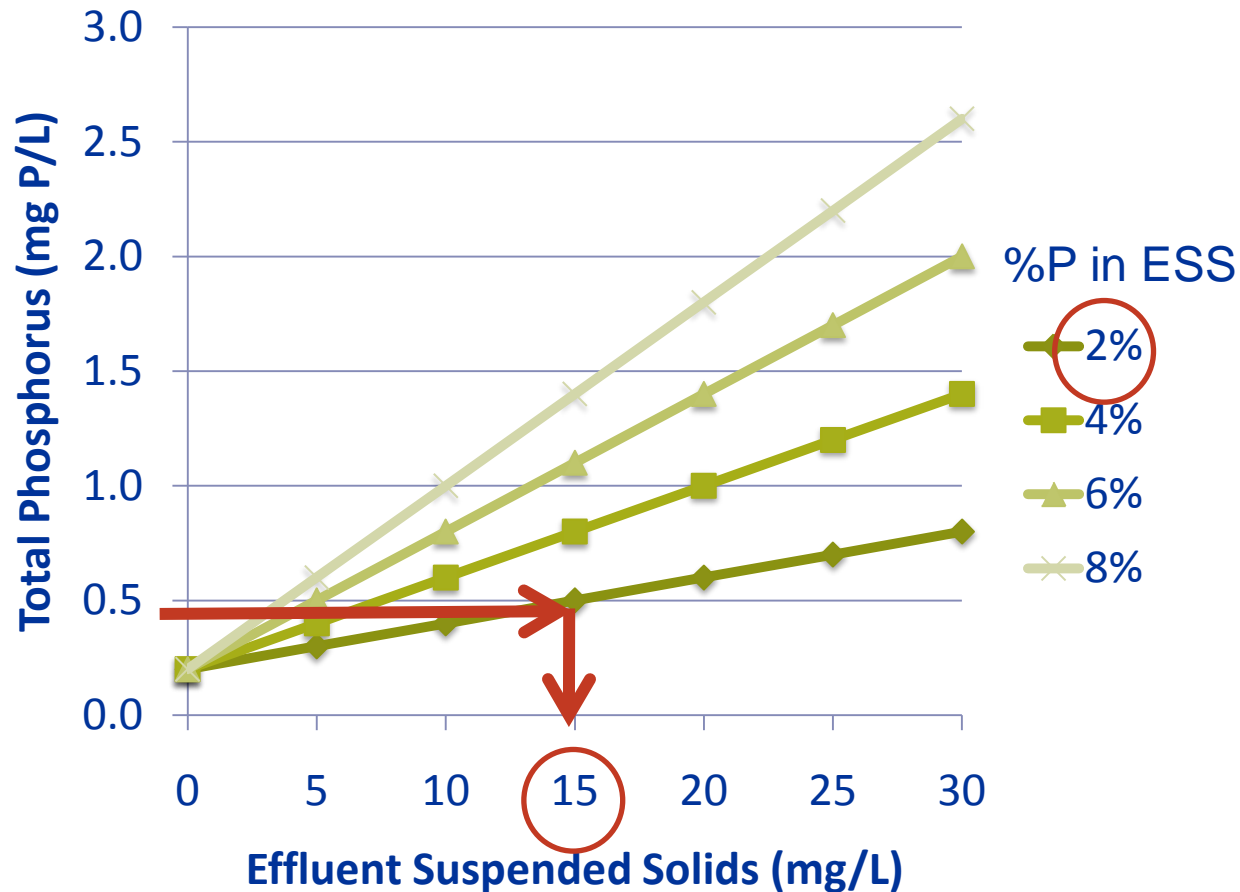
- All biological processes
- Incorporation of ortho-P into biomass during growth:  
 $C_{12}H_{87}O_{23}N_{12}P$
- Waste biomass P % depends on whether conventional activated sludge or Bio-P is used

# Removal Concepts: Incorporation into Biomass



# Removal Concepts: Incorporation into Biomass

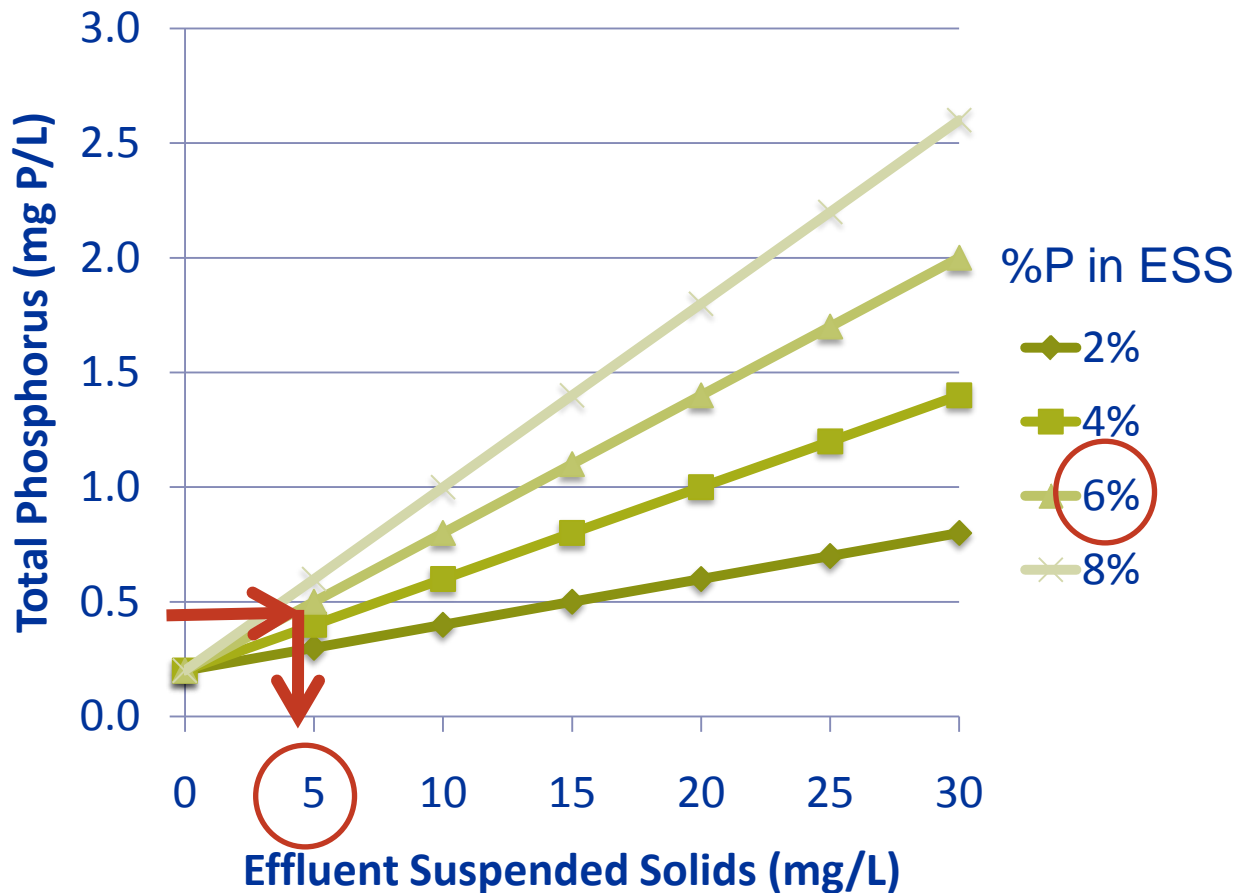
ESS needed for  $< 0.5$  mg/L TP with conventional activated sludge  
Assumes ortho-P = 0.2 mg P/L





# Removal Concepts: Incorporation into Biomass

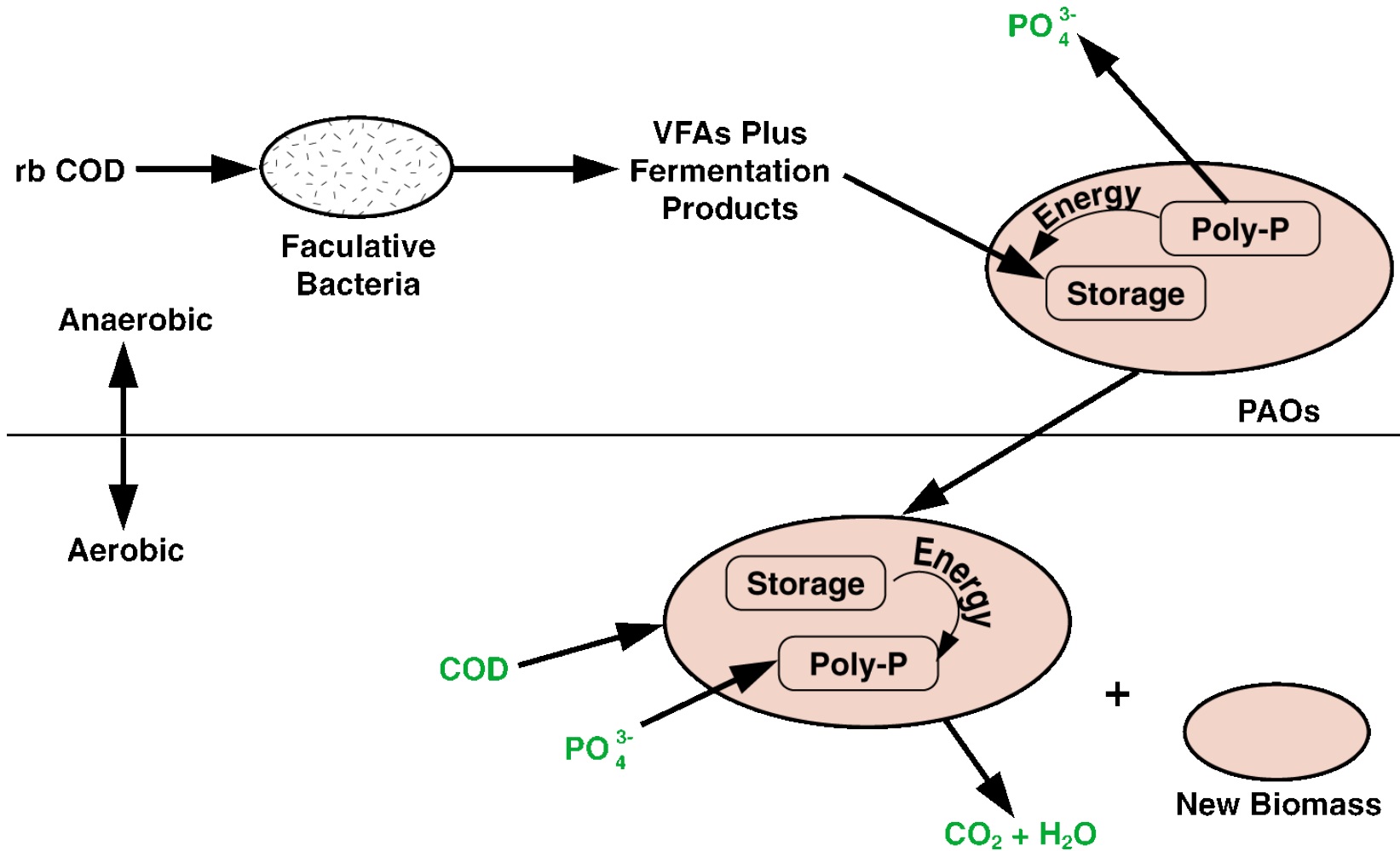
ESS needed for < 0.5 mg/L TP with Bio-P  
Assumes ortho-P = 0.2 mg P/L



# Removal Concepts: Bio-P

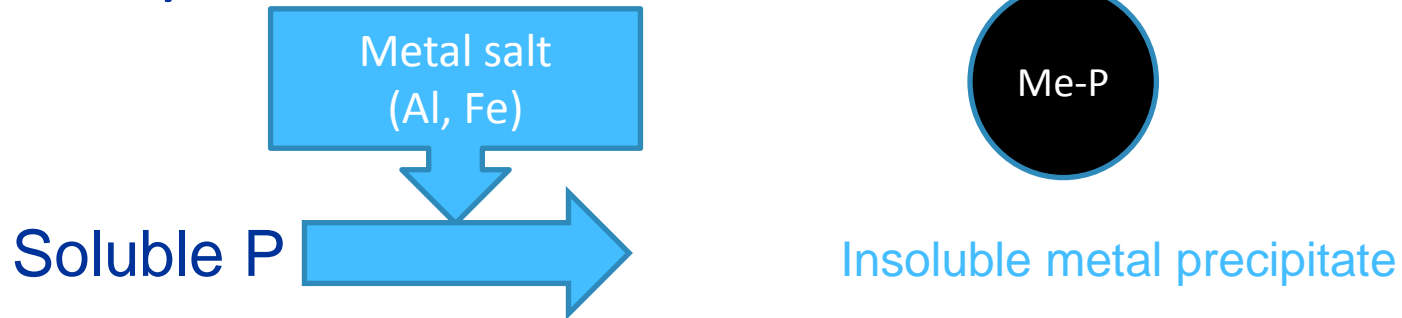
- Anaerobic (“no air” = no nitrate): release ortho-P
- Aerobic: take up more ortho-P than originally released
  - Performed by P-accumulating organisms or PAOs, distinct from “ordinary” heterotrophs

# Removal Concepts: Bio-P

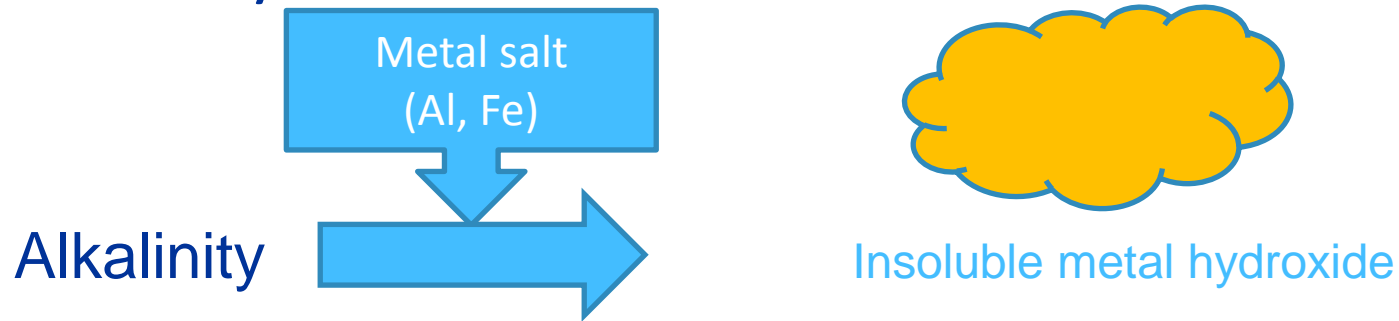


# Removal Concepts: Chemical Precipitation

- Primary reaction:

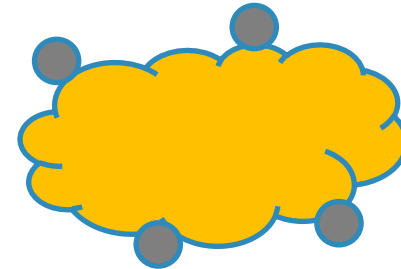
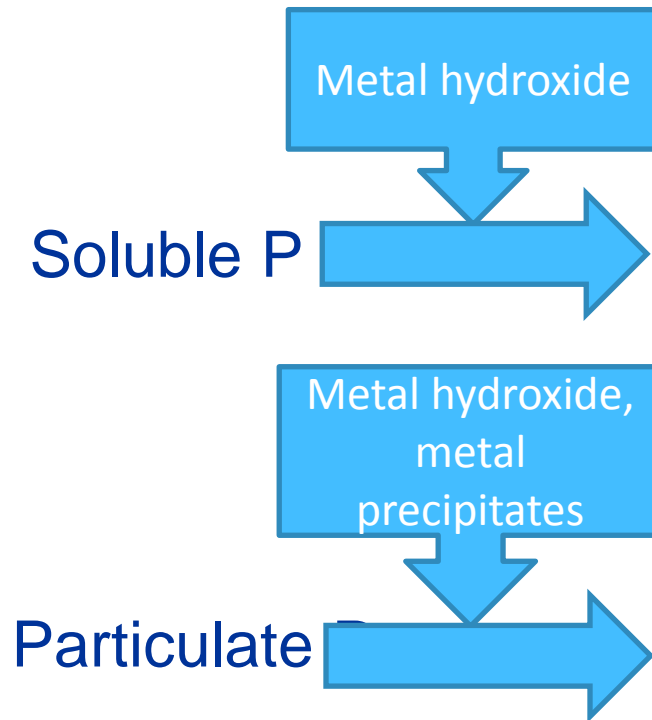


- Secondary reaction:

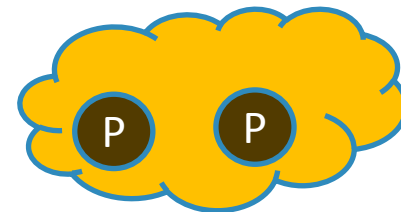


# Removal Concepts: Chemical Precipitation

- Additional reactions:



P adsorbed to insoluble metal precipitate



Particulate P enmeshed in precipitates and hydroxides

# Removal Concepts: Typical Chemicals

- Iron salts
  - Ferric salts
  - Ferrous salts
- Aluminum salts
  - Alum
  - Sodium aluminate
  - Poly-aluminum chloride (PACl)
- Lime
- Polymers

# Process Considerations: Conditions for Bio-P

- Anaerobic/aerobic cycling
- Adequate carbon
  - VFAs (acetate, propionate)
  - Readily biodegradable COD (rbCOD) that can be fermented to VFAs by ordinary heterotrophs
- Minimization of anaerobic re-release of P
- Minimization of competition from glycogen-accumulating organisms

# Process Considerations: Carbon Required

Ratio	Minimum to Achieve 1 mg/L TP with Bio-P
BOD:P	20:1
COD:TP	45:1
VFA:TP	10:1
rbCOD:TP	15:1

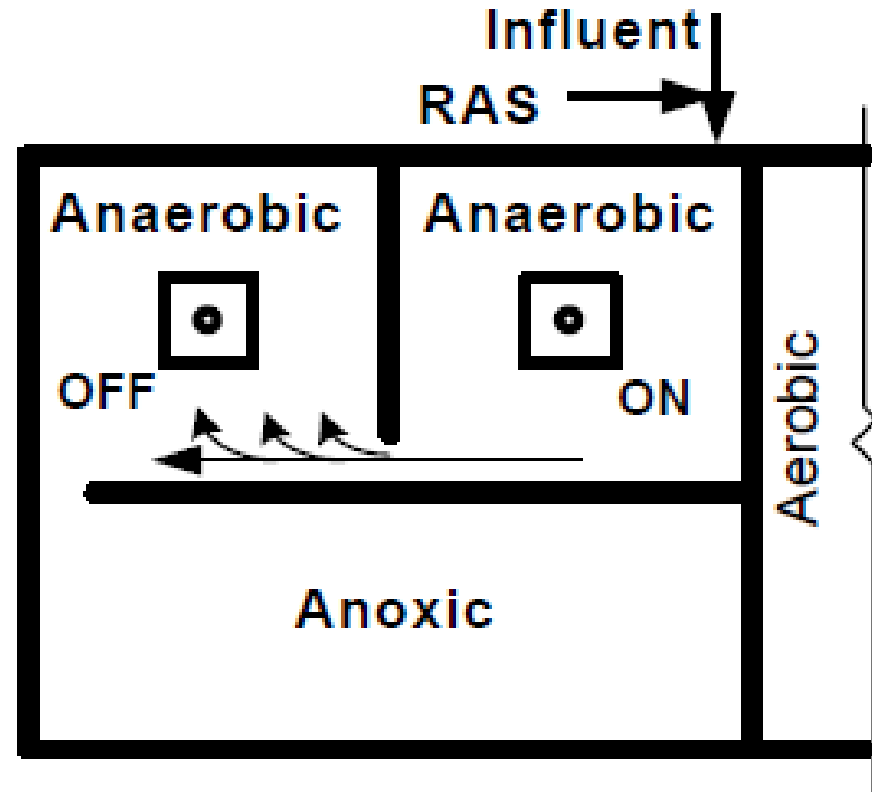


# Process Considerations: Carbon Sources

- Increase carbon with:
  - Sidestream fermentation of primary sludge
  - Carbon addition
  - Unmixed, inline fermentation (UMIF)
- Consider variability in VFA supply from:
  - Variable/high BOD removal in primary clarifiers
  - Wet weather flows
  - High/variable recycle loads

# Process Considerations: UMIF

- Pinery, CO
  - 1.5 mgd
  - 5-stage Bardenpho
  - Limited bio-P
- Switched off 2nd anaerobic mixer
- Allow MLSS to settle and ferment
- Influent TP = 9 mg/L
- Secondary effluent TP = 0.5 mg/L



Barnard et al. 2010. "Fermentation of mixed liquor for phosphorus removal" Presented at WEFTEC.

# Removal Concepts: Re-Release of P

- Re-release of stored P from Bio-P
- P assimilated into biomass or removed chemically does not release
- Re-release of P can occur:
  - In anoxic zone that becomes anaerobic
  - When aerobic digester is decanted after air turned off over night
  - When solids become anaerobic during thickening/dewatering
  - In anaerobic digester

# Process Considerations: Avoiding Re-Release

- Consider converting portion of initial anoxic zone to swing zone to avoid anaerobic conditions
- Consider conversion of second anoxic zone to aerobic
- Avoid carrying a deep clarifier sludge blanket
- Evaluate effects of P-rich sidestream and consider avoiding:
  - Unaerated sludge storage
  - Co-settling of primary sludge and WAS in primary clarifier
  - Anaerobic digestion

# Process Considerations: Avoiding GAO Competition

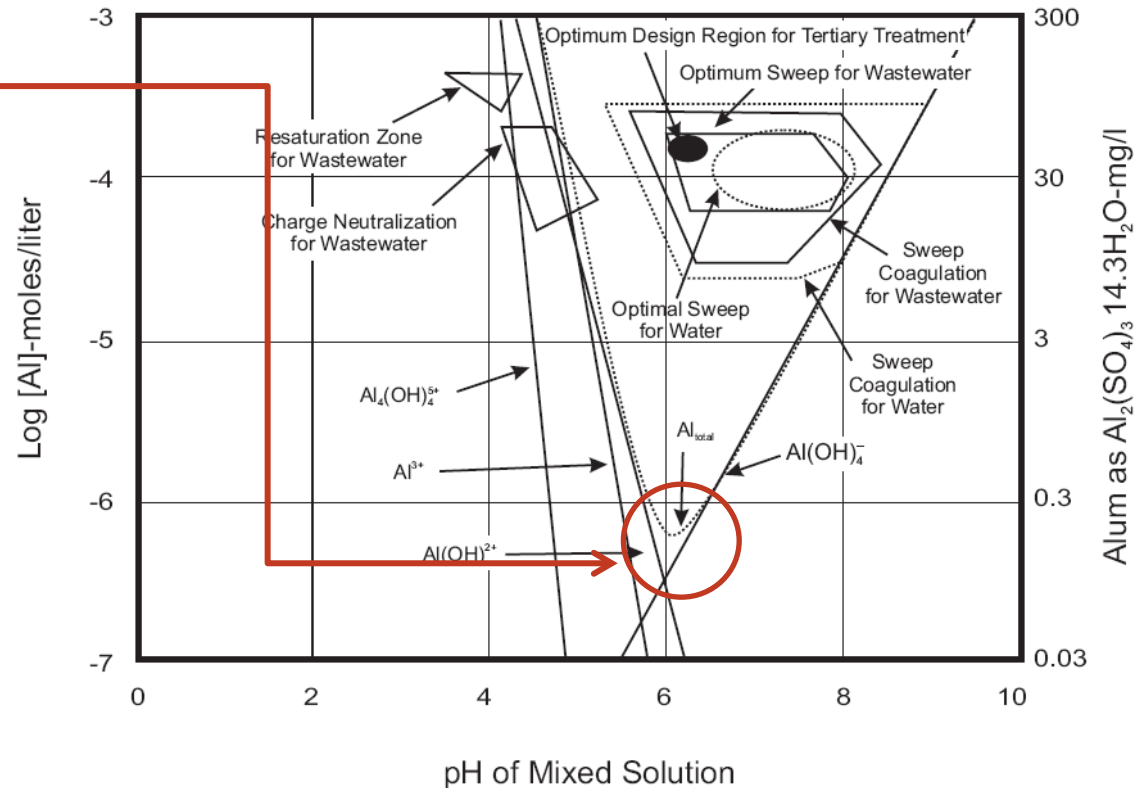
	Anaerobic	Aerobic
PAOs	<ul style="list-style-type: none"> <li>✓ VFA uptake and storage</li> <li>✓ P release</li> </ul>	<ul style="list-style-type: none"> <li>✓ Excess P uptake</li> <li>✓ Stored food oxidized</li> </ul>
GAOs	<ul style="list-style-type: none"> <li>✓ VFA uptake and storage</li> <li><u>No P release</u></li> </ul>	<ul style="list-style-type: none"> <li><u>No excess P uptake</u></li> <li>✓ Stored food oxidized</li> </ul>

# Process Considerations: Avoiding GAO Competition

- GAO conditions:
  - Warm temperatures
  - Long SRT
  - Long anoxic and anaerobic HRTs
  - Variable supply of VFAs
  - Ongoing use of acetic acid
  - pH < 7

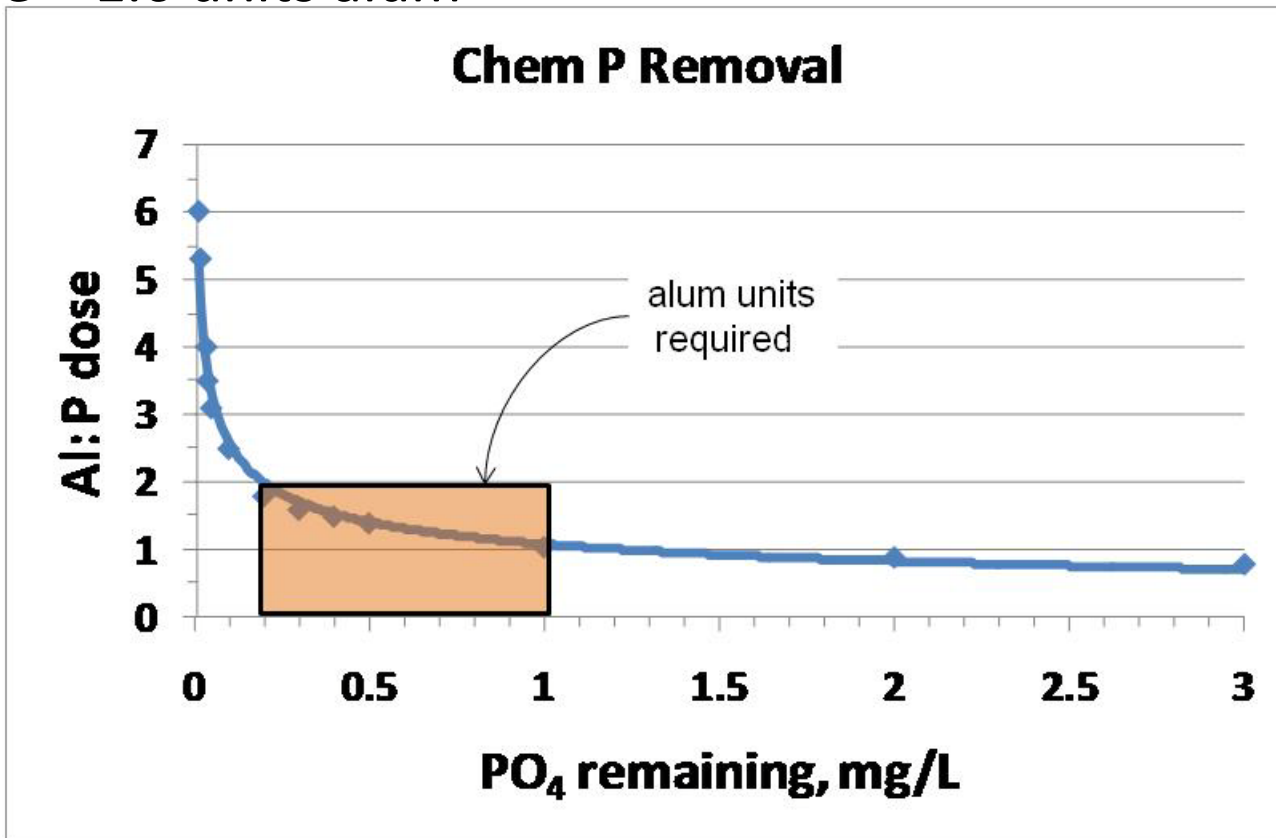
# Process Considerations: Conditions for Chemical P

- Optimal pH
- Adequate mixing
- Multiple addition points



# Process Considerations: Single-Point Addition

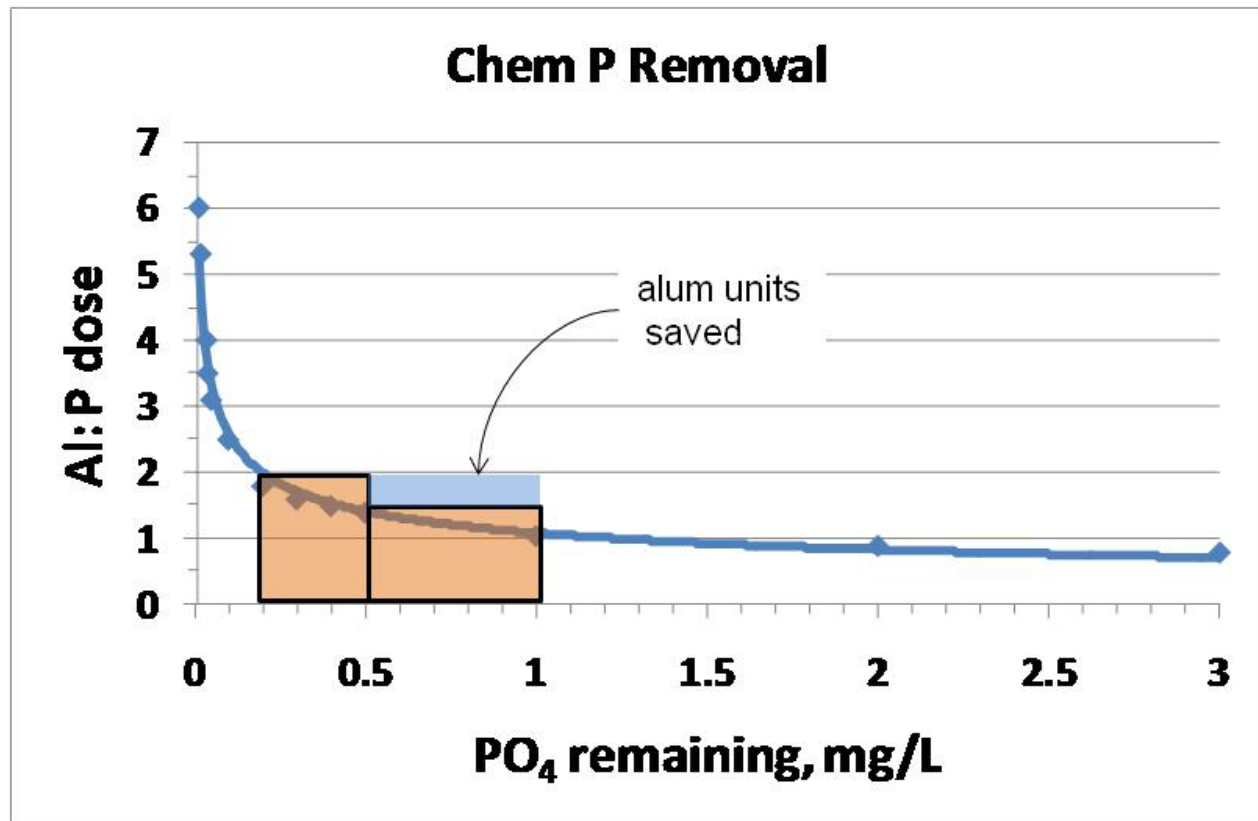
- 1 mg/L to 0.2 mg/L
- Dose = 1.6 units alum





# Process Considerations: Dual-Point Addition

- Stage 1:
  - 1 mg/L to 0.5 mg/L
- Stage 2:
  - 0.5 mg/L to 0.2 mg/L
- Dose = 1.35 units alum



2-stage dosing reduces alum demand by 16% in this example

# Process Considerations: Dual-Point Addition

- Example 1: Single feed removal
  - 1 mg/L to be reduced to 0.2 mg/L
  - 0.8 mg/L reduction requires 2.0:1 Al:P ratio
- Example 2: Dual feed removal
  - Stage 1: 1 mg/L reduced to 0.5 mg/L
  - 0.5 mg/L reduction requires 1.5:1 Al:P ratio
  - Stage 2: 0.5 mg/L reduced to 0.2 mg/L
  - 0.3 mg/L reduction requires 2.0:1 Al:P ratio
- 16% less chemical using dual feed

# Process Considerations: Effluent TP with Bio-P

- From Randall:
  - 0.16 mg/L at Bowie Creek, MD
  - ESS ~ 2 mg/L
- From Barnard:
  - 0.11 mg/L at Kalispell, MT
- Conventional wisdom:
  - 1 mg/L
  - Need filters

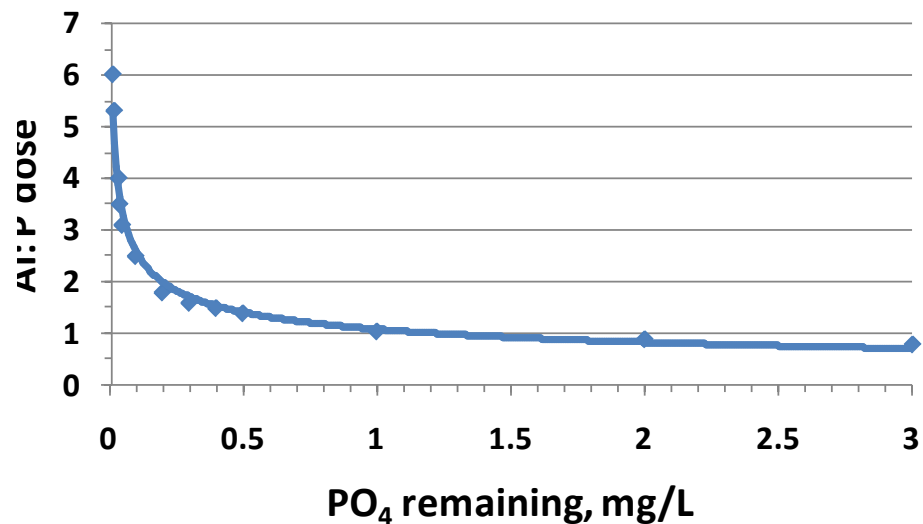
# Process Considerations: Effluent TP with Chemical P

- Precipitation before/with secondary treatment: 0.1 to 0.4 mg/L
- Tertiary clarification/filtration: 0.05 mg/L



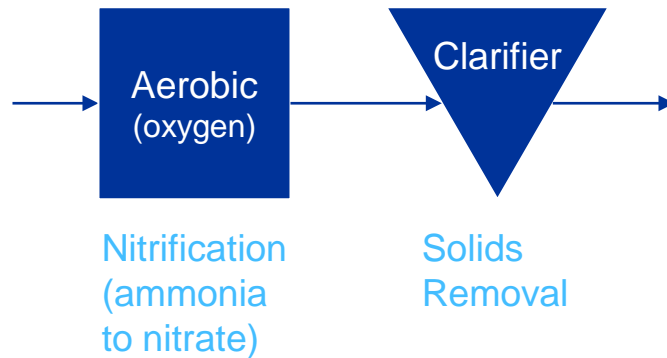
# Process Considerations: Balancing Bio-P and Chemicals

- Very difficult to avoid releasing P taken up during Bio-P
- Bio-P may reduce chemical use, but chemicals likely still needed
- Decision for chemicals is:
  - Treat large, dilute flow?
  - Treat small, concentrated flow (digester decant, filtrate)?



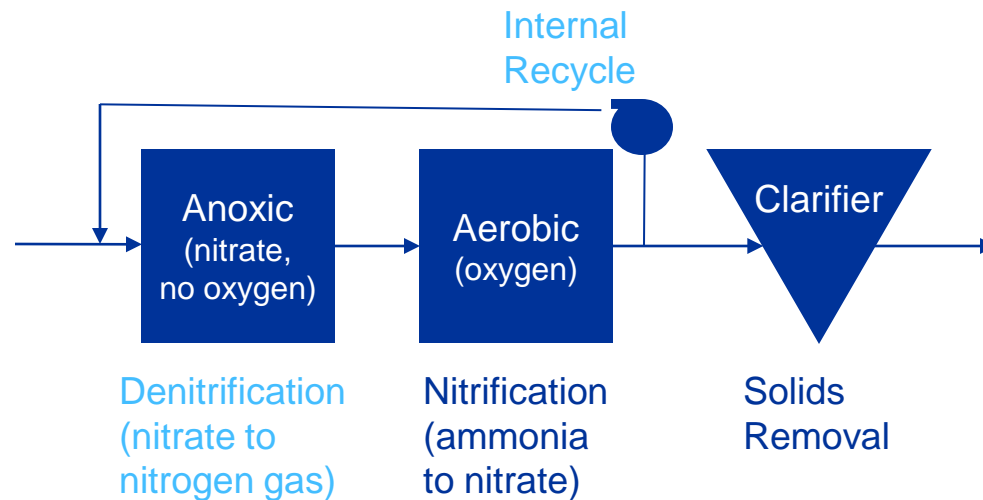
# N & P Removal: Combined Nutrient Removal

- **Nitrification (ammonia to nitrate)**



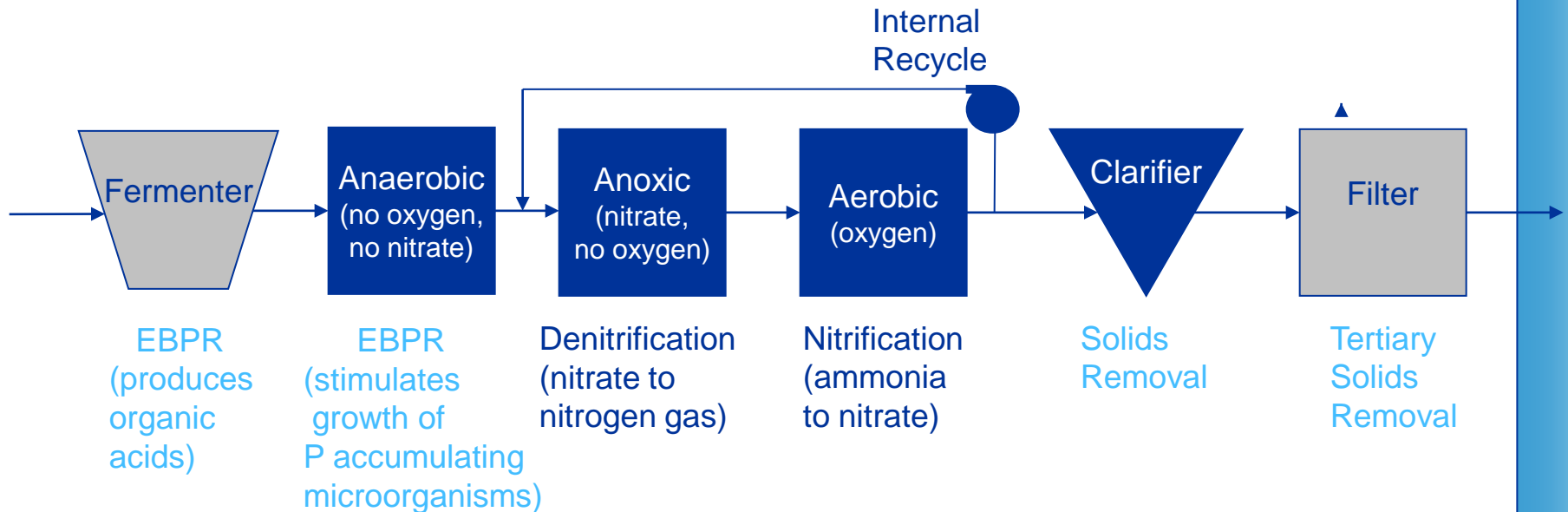
# N & P Removal: Combined Nutrient Removal

- Nitrification (ammonia to nitrate)
- **Denitrification (nitrate to nitrogen gas)**



# N & P Removal: Combined Nutrient Removal

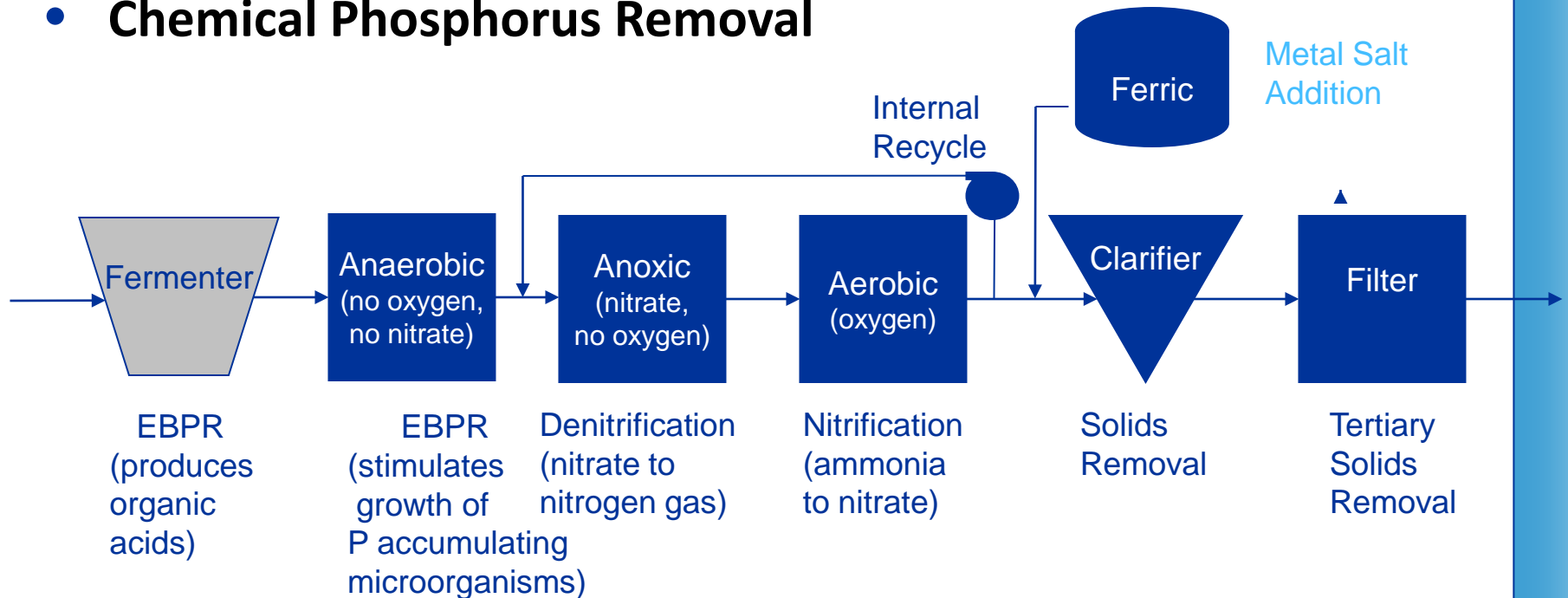
- Nitrification (ammonia to nitrate)
- Denitrification (nitrate to nitrogen gas)
- **Enhanced Biological Phosphorus Removal (EBPR)**





# N & P Removal: Combined Nutrient Removal

- Nitrification (ammonia to nitrate)
- Denitrification (nitrate to nitrogen gas)
- Enhanced Biological Phosphorus Removal (EBPR)
- **Chemical Phosphorus Removal**



# N & P Removal: Combined Nutrient Removal

- Nitrification (ammonia to nitrate)
- Denitrification (nitrate to nitrogen gas)
- Enhanced Biological Phosphorus Removal (EBPR)
- Chemical Phosphorus Removal
- **Improved Denitrification**

